

Application No.: 10/774154

Case No.: 58561US004

**Amendments to the Specification:**

Please amend the specification as follows:

On page 18, please replace the paragraph that starts on line 2 with the word "A" and ends on line 18 with the word "cycles" with the following amended paragraph:

A copolymer of TFE, HFP and VDF was prepared as follows:

A polymerization kettle with a total volume of 47.5 l equipped with an impeller agitator system was charged with 29.0 l deionized water; 2 g oxalic acid, 12 g ammonium oxalate and 252 g of a 30 weight % aqueous solution of perfluorooctanoate ammonium salt (FX 1006 of 3M Company, APFO). The oxygen free kettle was then heated up to 60° C and the agitation system was set to 240 rpm. The kettle was charged with ethane to a pressure of 1.1 bar absolute, 847 g hexafluoropropylene (HFP) to a pressure of 8.4 bar absolute, with 253 g ~~vinylidene fluoride~~ vinylidene fluoride (VDF) to 12.8 bar absolute and with 425 g tetrafluoroethylene (TFE) to 16.8 bar absolute reaction pressure. The polymerization was initiated by the addition of 25 ml 1.31% aqueous potassium permanganate (KMnO<sub>4</sub>) solution and a continuous feed of KMnO<sub>4</sub> ~~[[ - ]]~~ solution was maintained with a feed rate of 60 ml/h. As the reaction starts, the reaction temperature of 60°C was maintained and the reaction pressure of 16.8 bar absolute was maintained by the feeding TFE, VDF and HFP, into the gas phase with a feeding ratio HFP (kg)/TFE (kg) of 0.423 and a feeding ratio VDF (kg)/TFE (kg) of 0.820. When a total feed of 6610g TFE was reached in 185 min, the feed of the monomers was interrupted by closing the monomer valves. Within 10 minutes, the monomer gas phase was reacted down to a kettle pressure of 9.2 bar. Then the reactor was vented and flushed with N<sub>2</sub> in three cycles.

On page 22, please replace the paragraph that starts on line 3 with the word "The" and ends on line 15 with the word "cycles" with the following amended paragraph:

The polymerization kettle was first charged with 1750 g hexafluoropropene (HFP) to a pressure of 11 bar absolute, then the stainless steel cylinder with a total volume of 3.87 l used as feeding line for HFP was fully evacuated (150 mbar abs). After complete evacuation, the cylinder was charged to a pressure of 1.35 bar absolute with bromodifluoroethene (BDFE), which corresponds to 26.6 g at room temperature according to the ideal gas law. Then the cylinder was

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rapidly charged with 1290 g HFP in order to ensure a sufficient dispersion of BDFE into HFP under turbulent flow conditions. The polymerization was initiated by the addition of 38 g ~~ammoniumperoxodisulfate~~ ammonium peroxodisulfate (APS) in 100 ml deionized water. As the reaction starts, the reaction temperature of 70°C was maintained and the reaction pressure of 17 bar absolute was maintained by the feeding TFE and HFP into the gas phase with a feeding ratio HFP (kg)/TFE (kg) of 0.11. When a total feed of 10 kg TFE was reached in 275 min, the feed of the monomers was interrupted by closing the monomer valves. Then the reactor was vented and flushed with N<sub>2</sub> in three cycles.